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# Statistical Model for Melting Heat Transfer in Micropolar Nanofluid Flow over an Electromagnetic Actuator with Irregular Thickness

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#### **Abstract**

This article analyses statistical model mechanism in the motion of micropolar nanofluid over an electromagnetic actuator with variable thickness. The formulated model captures melting heat transfer phenomenon coupled with thermal radiation, viscous dissipation, thermal-movement and Brownian motion of nanoparticles. The model equations are restructured into ordinary derivatives from the initial partial derivatives by means of relevant similarity quantities. The equations are subsequently tackled numerically via shooting technique alongside Runge-Kutta Fehlberg scheme. The results are displayed graphically to showcase the contributions of the physical terms emerging from the model on the dimensionless quantities. In the analysis, it is found that an enhancement in the magnitude of the melting heat parameter reduces the surface heat propagation but viscous dissipation term acts contrary. Besides, augmenting the magnitude of micropolar and modified Hartmann number parameters boosts the fluid motion. More so, various statistical models are applied to test the data set for the coefficient of skin friction and the Nusselt number for variations in the micropolar fluid parameter (K). The statistical analysis points out that the data set for skin friction coefficient fits the Frechet model for K = 0 and the Weibull model for K = 1,2,3 whereas that of the Nusselt number fits the Frechet distribution for K = 0, 1 and Lognormal distribution for K = 2 & 3.

**Keywords:** Electromagnetic actuator, Microplar nanofluid; Melting heat transfer; Statistical model, Thermophoresis

### 1.0 Introduction

Eringen (1966, 1972) conceputualized the concept of micropolar fluid and thermomicropolar fluid respectively. Micropolar fluid is a branch of non-Newtonian fluid which posses microstructures with a unique characteristics of randomly oriented or rigid spherical particles. This fluid model accurately captures the flow

mechanism of animal blood, liquid crystals, polymeric suspensions, colloidal fluids and exotic lubricants (Lukaszewicz, 1999; Hayat *et al.*, 2008; Chen *et al.*, 2011, Fatunmbi and Adeniyan, 2018). Due to wide-ranging engineering and industrial applications derivable from micropolar fluid, various researchers have paid attention to investigate its flow mechanism

as well as its dynamics of heat transfer under diverse conditions and configurations. Its applications can be encountered in paint rheology and chemical engineering, bio-mechanics engineering (e.g. motion of blood in the body, fluid movement in the brain, etc.), the cooling of metallic sheet in water bath, etc. (Rahman, 2009; Reena and Rana, 2009).

different areas of manufacturing and engineering processes (e. g. transportation processes, pharmaceutical and drug delivery, cancer treatment, etc.), the concept of heating and cooling are often encountered. Hence, it becomes essential to investigate the thermal properties of various devices for performance. The suspension of nanometersized particles in the convectional fluid (such as: water, kerosene, oil, ethlene glycol, etc.) to form a colloidal solution of nanoparticles in the base fluid is termed nanofluid. Usually, these nanoparticles are typically made of metals, oxides, carbides, or carbon nanotubes, This new class of fluids have the capacity to enhance the thermal conduction as well as the thermophysical fluid properties (viscosity, thermal conductivity, thermal diffusivity, heat transfer). Choi (1995) initiated such a concept and due to wide applications of such phenomenon, various researchers have reported on their flow mechanism. Noor et al. (2015) carried out an analysis on the mixed convection of a micropolar nanofluid towards a stagnation point over an elongated surface. Their investigation showed that the blend of convectional fluid and the nanoparticles produced an enhanced heat transfer mechanism. Gangadhar et al. (2017) employed a numerical approach to evaluate the motion of magneto-micropolar nanofluid on dimensional stretching/shrinking material with surface mass flux featuring Newtonian heating condition. Subhani and Nadeem (2018) inspected the thermal characteristics and motion of micropolar hybrid nanoliquid in a porous material surface. The study showed that heat transfer in a hybrid naoliquid is higher than that of nanofluid in the presence of microrotation Atif et al. (2019)examined effects. bioconvective motion of micropolar fluid with the mixture of nanoparticles consisting motile microorganism and wall stratification. The authors pointed out that a rise in the micropolar material parameter caused a decline in the thermal field as well concentration profile. Recently, Fatunmbi and Salawu (2021) discussed a numerical analysis of chemically reacting micropolar nanofluid motion featuring viscous dissipation and multiple slips effects at the wall. The authors reported a shrinking concentration boundary layer but an enlarged momentum boundary structure in the presence of Brownian motion parameter. Of recent, Fatunmbi et al. (2021) evaluated heat transfer characteristics in the motion of tangent hyperbolic nanofluid over permeable expanding plate neighbourhood of a stagnation point in the presence of nonlinear mixed convection term. The researchers reported a drop in the heat transfer rate due to impovement in the magnitude of thermophoresis and the Brownian motion terms.

In engineering science such as in geophysics and astrophysics, the use of magnetic fields for the control of electro-conducting fluids as liquid metals, plasmas, etc. is important. However, when the electrical conductivity of the fluid is low, there is a need to introduce external electric field because the external magnetic field currents alone cannot induce efficient flow mechanism in scenarios. device known such electromagnetic actuator (Riga plate) can be used to induce the required flow current. In this device, there is arrangement of fixed alternating electrodes and magnets placed on the surface such that the Lorentz force is generated parallel to the plane. This idea was originated by Gailitis and Lielausis (1961) and has been extended by many scholars (Abbas et al., 2016; Fatunmbi and Adeosun, 2020; Fatunmbi et al., 2021). In all of these studies however, the application of statistical models to test the data set for the engineering quantities of interest (skin friction coefficient and the Nusselt number) and to fit the best distribution for variations in the fluid material property has not been considered. This becomes necessary to accurately predict the pattern of flow and heat transfer behaviour of fluid material property for applications in various industrial activities.

Hence, the intent of the current study is to establish statistical model for the flow and melting heat transfer in micropolar nanoliquid over an electromagnetic actuator with variable thickness. The developed model features the effects of viscous dissipation, thermal radiation and temperature-reliant thermal conductivity. This study therefore intends to provide answers to the following research questions. How does the modified Hartmann number affect the flow and thermal fields of the micropolar nanoliquid? Is there a significant impact of the variable thickness and melting heat transfer on the flow and thermal field of micropolar nanoliquid? Which statistical distribution model provides the best fit for the skin friction coefficient for variation in the micropolar fluid material? Which statistical distribution model provides the best fit for Nusselt number (heat transfer) for variation in the micropolar fluid material?

To provide answers to aforementioned questions, the controlling equations have been numerically integrated via the approach of shooting technique and associated with Runge-Kutta Fehlberg algorithm. Afterwards, various graphs have been plotted and tables generated to discuss the effects of the pertinent parameters affecting the flow dynamics and heat transfer mechanism.

# 2 Problem Development

An incompressible, steady motion and melting heat transfer of micropolar nanofluid over an electromagnetic actuator with variable thickness is considered. In the development of this problem, there is an assumption viscous thermophorseis dissipation, and Brownian motion effects are present whereas the thermal conductivity relies on the temperature. direction of motion is in x axis while y direction is fixed perpendicular to it with respective components of velocity indicated as u and v as displayed in figures 1a & 1b. The sheet is stretching with the velocity  $u = u_w(x) =$  $a(x+w)^n$ .

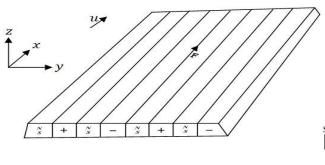


Figure 1a: Electromagnetic actuator

The sheet is not flat as described in Fig. 1b. with a given profile which is specified as  $y = b(x+w)^{(1-n)/2}$ , where b is taken so small for the sheet to be suitably thin. This problem is valid for  $r \neq 1$  since r = 1 depicts a flat sheet case. In the boundary conditions, the stretching surface temperature and concentration are higher than that of the free stream. i.e.  $T_w > T_\infty$  and  $C_w > C_\infty$ .

$$C_{W} > C_{\infty}.$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = (\mu + \kappa) \frac{\partial^{2} u}{\partial y^{2}} + \frac{\kappa}{\rho} \frac{\partial N}{\partial y} + \frac{\pi j_{0} M_{0}}{8\rho} \exp\left(-\frac{\pi}{h}y\right),$$

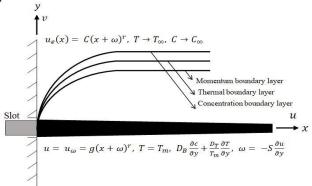


Figure 1b: Flow configuration and coordinate system

# 2.1 The Governing Equations

In line with the above-mentioned assumptions, the equations governing the problem are communicated as follows (see Fatunmbi and Adeosun, 2020; Iqbal *et al.*, 2017):

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0,\tag{1}$$

(2)

$$u\frac{\partial N}{\partial x} + v\frac{\partial N}{\partial y} = \frac{\gamma}{\rho_i}\frac{\partial^2 N}{\partial y^2} - \frac{\kappa}{\rho_i}\left(2N + \frac{\partial u}{\partial y}\right),\tag{3}$$

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \frac{1}{\rho c_p}\frac{\partial}{\partial y}\left(k\frac{\partial T}{\partial y}\right) + \Upsilon\left[\frac{D_T}{T_\infty}\left(\frac{\partial T}{\partial y}\right)^2 + D_b\left(\frac{\partial T}{\partial y}\frac{\partial C}{\partial y}\right)\right] + \frac{(\mu + \kappa)}{\rho c_p}\left(\frac{\partial u}{\partial y}\right)^2 + \frac{16\sigma^* T_\infty^3}{3k_\star \rho c_p}\frac{\partial^2 T}{\partial y^2},\tag{4}$$

$$u\frac{\partial c}{\partial x} + v\frac{\partial c}{\partial y} = D_b \frac{\partial^2 c}{\partial y^2}$$

$$+\frac{D_T}{T_{\infty}} \left( \frac{\partial^2 T}{\partial y^2} \right). \tag{5}$$

Subject to the following boundary conditions:

$$u = u_w(x) = a(x+w)^n, v = 0, T = T_m, D_b \frac{\partial C}{\partial y} + \frac{D_T}{T_m} \frac{\partial T}{\partial y} = 0, N = -m \frac{\partial u}{\partial y},$$

$$k \left(\frac{\partial T}{\partial y}\right) = \rho [\lambda_1 + C_s(T_m - T_0)] v(x,0) \text{ at } y = b(x+w)^{(1-n)/2},$$

$$u \to 0, T \to T_\infty, C \to C_\infty \text{ } y \to \infty.$$

$$(6)$$

The variation of the thermal conductivity with temperature is expressed as (see Hayat et .al, 2018)

$$k = k_{\infty} \left( 1 + L \frac{T - T_m}{T_{\infty} - T_m} \right). \tag{7}$$

The quantities in Eq. (8) are introduced into the main equations to transform them from partial to ordinary differential equations (see Hayat et .al, 2018).

$$K = \left(\frac{\kappa}{\mu}\right), Ec = \left(\frac{u_{w}^{2}}{c_{p}(T_{\infty}-T_{m})}\right), \quad Le = \left(\frac{\alpha}{D_{b}}\right), \epsilon = \left[\frac{\pi}{h}\left(\frac{2\nu(x+w)^{1-n}}{(r+1)a}\right)^{\frac{1}{2}}\right], \quad Nt = \frac{D_{T}Y(T_{\infty}-T_{m})}{\nu T_{\infty}}, \quad \alpha = \left(\frac{\kappa}{(\mu c_{p})}\right), \quad \xi = y\left[\frac{(n+1)}{2\nu}a(x+w)^{n-1}\right]^{\frac{1}{2}}, u = a(x+w)^{n}F'(\xi), N = G(\xi)\left[\frac{a^{3}(n+1)(x+w)^{(3n-1)}}{2\nu}\right]^{\frac{1}{2}}, Pr = \left(\frac{\nu}{\alpha}\right), \quad Nb = \frac{D_{b}YC_{\infty}}{\nu}, \nu = -\left[\frac{a\nu(r+1)}{2}(x+w)^{(r-1)}\right]^{\frac{1}{2}}\left(F(\xi) + \frac{(n-1)}{(r+1)}\eta F'(\xi)\right), Z = \left(\frac{c_{p}(T_{\infty}-T_{m})}{[\lambda_{1}+c_{s}(T_{m}-T_{0})]}\right), \gamma = \left(\mu + \frac{\kappa}{2}\right)j, \quad j = \left(\frac{\nu}{n}\right)x^{(1-n)}, \quad \Phi(\eta) = \frac{c}{C_{\infty}},$$

$$v = -\left[\frac{a\nu(n+1)}{2}(x+w)^{(r-1)}\right]^{\frac{1}{2}}\left(F(\xi) + \frac{(n-1)}{(n+1)}\eta F'(\xi)\right), \qquad \epsilon = \left[\frac{\pi}{h}\left(\frac{2\nu(x+w)^{1-r}}{(r+1)a}\right)^{1/2}\right], M = \left(\frac{\pi j_{0}M_{0}}{8na^{2}(x+w)^{2r-1}}\right), Nr = \frac{16\sigma^{*}T_{\infty}}{k_{s},k_{s}}, \epsilon = (1+L\theta).$$

$$(8)$$

The governing equations therefore translate to the underlisted equations in view of Eqs. (7) and (8).

$$(1+K)F''' - \left(\frac{2r}{r+1}\right)F'^2 + FF' + Kg' + \left(\frac{2}{r+1}\right)Me^{-\eta\epsilon} = 0,$$
(9)

$$(1+K/2)G'' + FG' - \left(\frac{3r-1}{r+1}\right)F'g - K(2g+F'')\left(\frac{2}{r+1}\right) = 0,$$
(10)

$$(1 + Nr + \epsilon \Theta)\Theta'' + \epsilon \Theta'^{2} + \Pr(F\Theta' + Ec(1 + K)F''^{2} + Nt\Theta'^{2} + Nb\Theta'\Phi') = 0, \tag{11}$$

$$\Phi'' + \frac{NT}{ND}\Theta'' + PrLeF\Phi' = 0. \tag{12}$$

$$F'(\beta) = 1, \Theta(\beta) = 0, \Phi(\beta) = 0, G = -mF''(\beta) \text{ at } \beta = b \left(\frac{(r+1)n}{2\nu}\right)^{1/2}$$
Subject to:
$$Z\Theta'(\beta) + PrF(\beta) = \beta \left(\frac{1-n}{1+n}\right)F'(\beta) \text{ at } \beta = b \left(\frac{(r+1)n}{2\nu}\right)^{1/2}$$

$$F'(\infty) \to 0, \Theta(\infty) \to 1, \Phi(\infty) \to 1 \text{ as } a \to \infty.$$
(13)

In Eqs. (9-13), the differentiation is done with respect to  $\xi$ ,  $\beta = \left(b\left(\frac{(n+1)a}{2\nu}\right)^{1/2}\right)$  is the wall thickness term and  $\xi = \beta = a\left(\frac{(n+1)\kappa}{2\nu}\right)^{1/2}$  denotes flat surface. In order to convert the domain into  $[0, \infty]$ , it is assumed that  $F(\xi) = f(\xi - \beta) = f(\eta)$ ,  $G(\xi) = g(\xi - \beta) = g(\eta)$ ,  $\Theta(\xi) = \theta(\xi - \beta) = \theta(\eta)$  and  $\Phi(\xi) = \phi(\xi - \beta) = \phi(\eta)$ , with these relations, the outlining equations simplify to:

$$(1+K)f''' - \left(\frac{2n}{n+1}\right)f'^2 + ff'' + Kg' + \left(\frac{2}{n+1}\right)Me^{-(a+\eta)h} = 0,$$
(14)

$$(1+K/2)g'' + fg' - \left(\frac{3n-1}{n+1}\right)f'g - K(2g+f'')\left(\frac{2}{n+1}\right) = 0,$$
(15)

$$(1 + Nr + L\theta)\theta'' + L\theta'^2 + Prf\theta' + PrEc(1 + K)f''^2 + PrNt\theta'^2 + PrNb\theta'\phi' = 0$$
(16)

$$\phi'' + \frac{Nt}{Nh}\theta'' + PrLef\phi' = 0. \tag{17}$$

Subject to:

at 
$$\eta = 0$$
  $f' = 1, \theta = 0, g = -mf'', \phi = 0, f = 1/\Pr\left[a\left(\frac{1-n}{1+n}\right) - Z\theta'\right]$   
as  $\eta \to \infty$   $f' \to 0, g \to 0, \theta \to 1, \phi \to 1$ . (18)

Table 1: Nomenclature

Symbol	Description	Symbol	Description
u, v	velocity in $x, y$ direction	$T_m$	melting temperature
ho	fluid density viscosity	h	width of magnets and electrodes
μ	dynamic viscosity	ν	fluid kinematic viscosity
$\kappa$	vortex viscosity	$\lambda_1$	latent fluid heat
T	Fluid temperature	$k^*$	mean absorption coefficient
$(\rho c_p)$	heat capacity	$C_s$	heat capacity of concentration surface
$a^{\dot{\star}}$	Stefan-Boltzmann constant	$T_0$	solid surface temperature
$T_{\infty}$	temperature at free stream	m	boundary parameter
k	Fluid thermal conductivity	$D_b$	molecular diffusivity
j	micro inertia density	$D_T$	Thermophoresis coefficient
L	thermal conductivity parameter	N	component of micro rotation
$u_w$	stretching velocity	γ	spin gradient viscosity
M	Modified Hartmann number	$\ddot{Z}$	Melting heat parameter
Ec	Eckert number	Le	Lewis number
K	Micropolar parameter	Nt	Thermophoresis term
Pr	Prandtl number	Nb	Brownian motion parameter
$\epsilon$	Dimensionless parameter	n	Power law index

#### 3. Numerical Method.

A numerical solution of the set of the boundary value problem Eqs. (14-18) has been sought due to strong nonlinearity of the problem. An unconditionally stable numerical solution via Runge-Kutta-Fehlberg scheme alongside with the shooting technique is employed. The detailed procedure of this method can be obtained in Xu

and Lee (2013); Mahanthesh *et al.* (2018); Fatunmbi and Okoya (2020).

# 3.1 Statistical Model selection

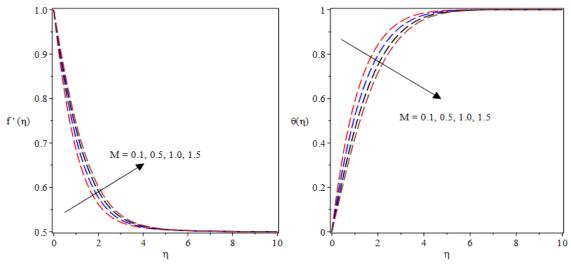
In this study, Akaike Information Criterion (AIC) and Bayesian Information Criterion (BIC) are employed to select the best statistical model (Shafiq *et al.*, 2021). The data for the skin friction coefficient  $C_{fx}$  and the Nusselt number

 $Nu_x$  are tested using AIC and BIC. The model that fits best to the data among basic statistical models listed in Table 2 is then determined via AIC and BIC for each model in the table. The distribution with the lowest BIC/AIC value is adjudged the best fitted.

The respective formula for AIC and BIC are:

#### 3.0 Results and Discussion

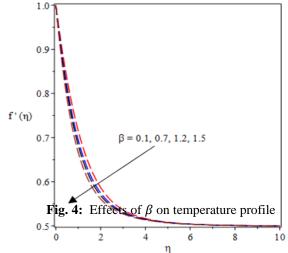
The effects of some selected physical parameters on the velocity field and heat distribution are graphically presented and discussed in this section. Figure 2 describes the impact of melting heat transfer M on the velocity. It is noticed that



 $AIC = -2\log(s) + 2c$  and  $BIC = -2\log(s) + c\log(n)$ 

Where *s* indicates the model likelihood function and *c* denotes number of parameters.

the fluid velocity enhances with growth in the magnitude of the melting parameter M within the boundary layer region.



**Fig. 2:** Effects of M on velocity profile

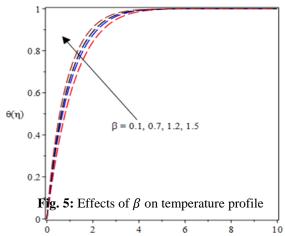
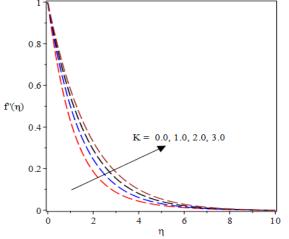


Fig. 3: Plot of M on temperature trend is attributed to the movement of the solid surface and the free stream in the same direction. Conversely, the thermal field witnesses a decrease in the heat distribution with growing values of M as depicted in Fig. 3

Figure 4 portrays the reaction of the velocity profile for growth in different values of the wall thickness parameter  $\beta$ . A decreased in the fluid motion is observed as the wall thickness parameter  $\beta$  rises. An increase in  $\beta$  depletes the momentum boundary layer structure which in turn propels a slow motion. It is shown that the velocity profile manifests a decreasing pattern

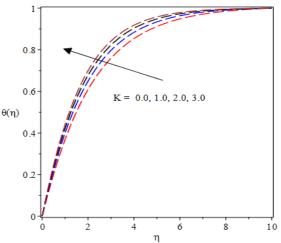
parameter K promotes an increase in the velocity profile as seen in Fig. 6. This is an indication that there is a reduction in the dynamic fluid viscosity as K increases. Nevertheless, the temperature distribution reduces for higher magnitudes of K as observed in Fig. 7.



with an increment in the wall thickness term

**Fig. 6.** Effects of *K* on temperature profile

**Fig. 8.** Effects of *H* on temperature profile

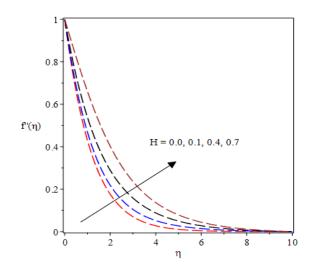


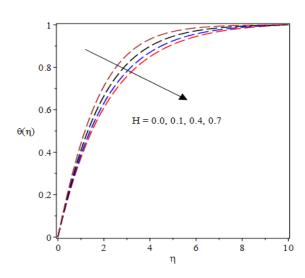
temperature distribution increases as  $\beta$ . A rise in

the magnitude of the micropolar material

**Fig. 7.** Effects of *K* on temperature profile

**Fig. 9.** Effects of *H* on temperature profile





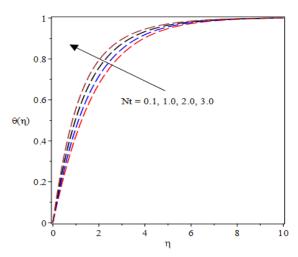
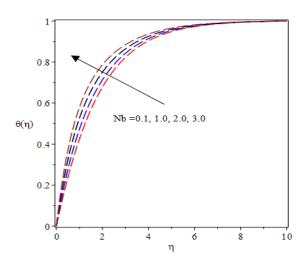


Fig. 10. Effects of Nt on temperature profile

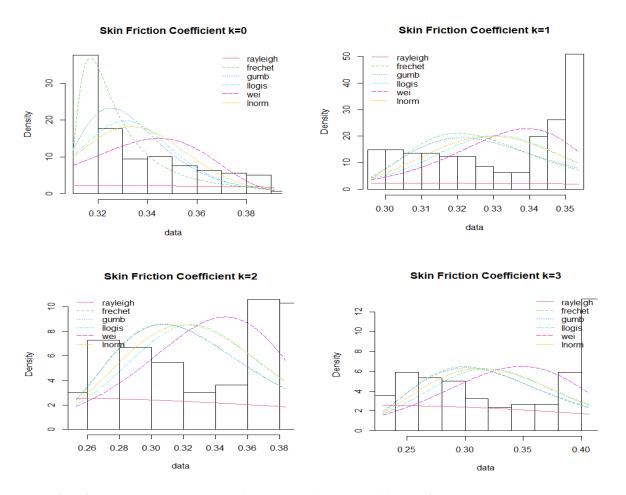
Figure 8 depicts the graph of the velocity profile for variation in the modified Hartmann number H. It is noticed that growing values of H boosts the hydrodynamic boundary layer and accelerates the fluid motion. The Lorentz force parallel to the wall induces current in the fluid such that there is a higerrr velocity due to rising values of H.

Figure 10 elucidates the impact of the thermophoresis parameter on the temperature profile  $\theta(\eta)$ . It is evident that growing values of Nt boosts the surface temperature as depicted in this figure. The thermal field expands due to thermophoresis occurrence owing to Brownian motion of the nanoparticles in fluids with a constant gradient of temperature. Similarly, the heat distribution also increases due to a rise in the Brownian motion which characterizes the haphazard motion of the nanoparticles as shown in Fig. 11.



**Fig. 11.** Effects of *Nb* on temperature profile

The data for the skin friction coefficient and Nusselt were further analyzed on the basis of Fig. 12 and 13, in order to obtain the statistical properties for the tested models. Tables 3 and 5 present the estimated parameters of the different distributions that have been tested with the considered data. Tables 4 and 6 give the AIC and BIC for the  $C_{fx}$  and  $Nu_x$  numbers. The result of AIC and BIC show that data set for  $C_{fx}$  fits the Frechet model for K = 0 and the Weibull model for K = 1,2,3. On the other hand,  $Nu_x$  data set fits the Frechet distribution well for K = 0.1 and the Lognormal distribution for K = 2,3. This is an indication that the form of the distribution changes after K = 0 for  $C_{fx}$  and K = 1 for  $Nu_x$ respectively. Figures 12 and 13 show the estimated densities using data of  $C_{fx}$  and  $Nu_x$ under the models in Table 1 which corroborate the results of the AIC and BIC.



**Fig. 12:** The estimated densities for the skin friction coefficient  $C_{fx}$ 

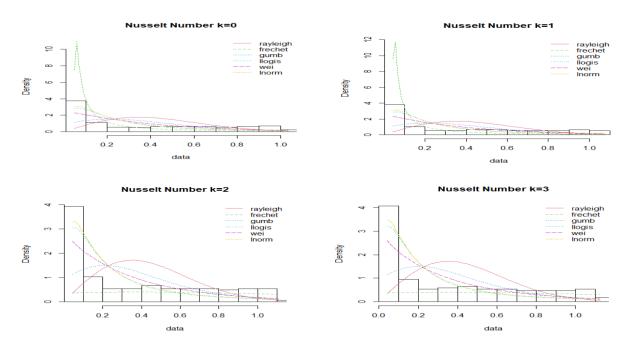


Fig. 13: The estimated densities for the Nusselt number  $Nu_x$ 

**Table 2:** The test distribution for skin friction coefficient  $C_{fx}$  and Nusselt number  $Nu_x$ 

	j.v
Distribution	Probability distribution function $f(x)$
Rayleigh	$f(x,\sigma) = \frac{x}{\sigma^2} e^{-\frac{x^2}{2\sigma^2}} ; x > 0, \sigma > 0$
Fre'chet	$f(x,\alpha,s,m) = \frac{\alpha}{s} \left(\frac{x-m}{s}\right)^{-1-\alpha} e^{-\left(\frac{x-m}{s}\right)^{-\alpha}}  ;  x > m, \ \alpha > 0, s > 0$
Gumbel	$f(x,\mu,\beta) = e^{-(z+e^{-z})}$ where $z = \frac{x-\mu}{\rho}$ ; $\mu > 0, \beta > 0$
Log-logistic	$f(x,\alpha,\beta) = \frac{\left(\frac{\beta}{\alpha}\right)\left(\frac{x}{\alpha}\right)^{\beta-1}}{\left(1+\left(\frac{x}{\alpha}\right)^{\beta}\right)^{2}}  ;  x > 0, \alpha > 0, \beta > 0$
Weibull	$f(x,\lambda,k) = \frac{k}{\lambda} \left(\frac{x}{\lambda}\right)^{k-1} e^{-\left(\frac{x}{\lambda}\right)^k} ;  x > 0, \lambda > 0, k > 0$
Log-normal	$f(x,\sigma,\mu) = \frac{1}{x\sigma\sqrt{2\pi}}e^{\left(-\frac{(\ln x - \mu)^2}{2\sigma^2}\right)}  \sigma > 0, \mu > 0$

**Table 3:** Parameter estimates for the statistical distribution of  $C_{fx}$ 

Skin friction coefficient $C_{fx}$						
Distribution	Parameter	K = 0	K = 1	K = 2	K = 3	
Rayleigh	σ	0.2376	0.2345	0.2363	0.2392	
	m	0.3008	-97251.9	-39700.7	-2042024	
Frechet	S	0.0206	97252.2	39701.0	2042024	
	α	1.8112	5586371.1	927900.6	35887025	
Gumbel	μ	0.3252	0.3209	0.3073	0.3001	
	β	0.0158	0.0190	0.0431	0.0579	
Log-logistic	β	26.3002	26.8173	11.1662	8.1042	
	α	0.3320	0.3319	0.3300	0.3289	
	k	14.105	21.0749	8.6823	6.2428	
Weibull	λ	0.3465	0.3401	0.3510	0.3586	
Log normal	μ	-1.0948	-1.1072	-1.1162	-1.1211	
	σ	0.0654	0.0605	0.1444	0.1987	

**Table 4:** Akaike Information Criterion (AIC) and Bayesian Information Criterion (BIC) for  $C_{fx}$ 

Skin friction coefficient $C_{fx}$						
Distribution		K =0	K =1	K = 2	K = 3	
	AIC	-245.763	-253.38	-251.87	-248.00	
Rayleigh	BIC	-242.694	-250.30	-248.77	-244.87	
Frechet	AIC	-820.387	-774.23	-521.01	-431.55	
	BIC	-811.181	-764.98	-511.69	-422.16	
	AIC	-793.898	-778.29	-523.02	-433.63	
Gumbel	BIC	-787.760	-772.12	-516.81	-427.37	
	AIC	-753.396	-781.76	-516.31	-422.59	
Log-logistic	BIC	-747.258	-775.60	-510.10	-416.33	
	AIC	-711.008	-816.70	-549.21	-454.14	
Weibull	BIC	-704.870	-810.54	-543.00	-447.88	
	AIC	-760.185	-798.60	-534.64	-441.59	
Log normal	BIC	-760.185	-792.43	-528.43	-435.33	

**Table 5:** Parameter estimates for the statistical distribution of  $Nu_x$ 

Nusselt number $Nu_x$						
Distribution	Parameter	K =0	K =1	K = 2	K = 3	
Rayleigh	σ	0.3456	0.3530	0.3539	0.3531	
	m	0.0448	0.0428	-5.4444	-5.4444	
Frechet	S	0.0487	0.0435	5.9444	5.9444	
	α	0.5999	0.5558	6.3889	6.3889	
Gumbel	μ	0.2137	0.2148	0.2083	0.2029	
	β	0.2376	0.2440	0.2451	0.2443	
Log-logistic	β	1.4581	1.4088	1.3691	1.3490	
	α	0.2146	0.2131	0.2022	0.1941	
	k	1.0472	1.0182	0.9815	0.9595	
Weibull	λ	0.3709	0.3719	0.3615	0.3530	
Log normal	μ	-1.5347	-1.5495	-1.5957	-1.6300	
	σ	1.09119	1.1306	1.1630	1.1801	

**Table 6:** Akaike Information Criterion (AIC) and Bayesian Information Criterion (BIC) for  $C_{fx}$ 

		• •	•		, ,	
Nusselt number $Nu_x$						
Distribution		K = 0	K = 1	K = 2	K = 3	
	AIC	132.3096	152.3221	172.9782	187.1494	
Rayleigh	BIC	135.3785	155.4035	176.0842	190.2793	
Frechet	AIC	-25.8300	-19.9633	333.1634	341.5887	
	BIC	-16.6230	-10.7191	342.4812	350.9784	
	AIC	66.0602	75.4469	80.4107	82.6341	
Gumbel	BIC	72.1980	81.6098	86.6226	88.8939	
	AIC	14.7996	21.3907	15.9855	9.6307	
Log-logistic	BIC	20.9374	27.5535	22.1974	15.8905	
	AIC	0.0728	4.9620	0.9057	-4.0227	
Weibull	BIC	6.2107	11.1248	7.1176	2.2371	
	AIC	-5.0487	1.4740	-4.4967	-11.3515	
Log normal	BIC	1.0891	7.6367	1.7151	-5.0917	

# **4.0 Concluding Remarks**

The present study evaluates statistical model for the flow and melting heat transfer in microplar nanoliquid over an electromagnetic actuator with variable thickness. The developed model features the effects of viscous dissipation, thermal radiation, temperature-based thermal conductivity. Main equations describing the physical problem are remodeled into ordinary differential equations using appropriate similarity transformation. The resultant equations have been tackled numerically via shooting technique alongside Runge-Kutta Fehlberg algorithm. Various statistical distributions such as Rayleigh,

Frechet, Gumbel, Log-logistic, Weibull, Log normal are applied to test the data set of the skin friction coefficient and the Nusselt number for variations in the micropolar nanofluid material parameter. In addition, Akaike Information Criterion (AIC) and Bayesian Information Criterion (BIC) were used to select the best statistical model. The results show that:

 The momentum boundary layer expands with melting heat transfer, modified Hartmann number and fluid material term whereas the fluid velocity decelerates with a rise in the magnitude of the wall thickness parameter.

- The thermal field as well as the temperature boundary layer improves with an increase in the Eckert number, thermophoresis and Brownian motion and micropolar fluid term.
- The data set for the skin friction coefficient fits the Frechet model in the absence of micropolar fluid (K = 0) and the Weibull model for K = 1,2,3 whereas that of the Nusselt number fits the Frechet distribution for K = 0,1 while Lognormal distribution fits for K = 2 and 3.
- The statistical model reveals that the form of the distribution for the data sets of skin friction coefficient and Nusselt number change after some values of material micropolar parameter.

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